- (4) The procedures in Method 19 shall be used to compute each 1-hour average concentration in ng/J (1b/million Btu) heat input.
- (i) The owner or operator shall use methods and procedures in this paragraph to conduct monitoring system performance evaluations under \$60.13(c) and calibration checks under \$60.13(d). Acceptable alternative methods and procedures are given in paragraph (j) of this section.
- (1) Methods 6, 7, and 3B, as applicable, shall be used to determine O_2 , SO_2 , and NO_x concentrations.
- (2) SO_2 or NO_x (NO), as applicable, shall be used for preparing the calibration gas mixtures (in N_2 , as applicable) under Performance Specification 2 of appendix B of this part.
- (3) For affected facilities burning only fossil fuel, the span value for a continuous monitoring system for measuring opacity is between 60 and 80 percent and for a continuous monitoring system measuring nitrogen oxides is determined as follows:

Fossil fuel	Span value for nitro- gen oxides (ppm)
Gas Liquid Solid Combination	500 500 1,000 500 (x+y)+1,000z

where:

- \boldsymbol{x} is the fraction of total heat input derived from gaseous fossil fuel,
- y is the fraction of total heat input derived from liquid fossil fuel, and
- z is the fraction of total heat input derived from solid fossil fuel.
- (4) All span values computed under paragraph (b)(3) of this section for burning combinations of fossil fuels are rounded to the nearest 500 ppm.
- (5) For affected facilities burning fossil fuel, alone or in combination with non-fossil fuel, the span value of the sulfur dioxide continuous monitoring system at the inlet to the sulfur dioxide control device is 125 percent of the maximum estimated hourly potential emissions of the fuel fired, and the outlet of the sulfur dioxide control device is 50 percent of maximum estimated hourly potential emissions of the fuel fired.
- (j) The owner or operator may use the following as alternatives to the ref-

erence methods and procedures specified in this section:

- (1) For Method 6, Method 6A or 6B (whenever Methods 6 and 3 or 3B data are used) or 6C may be used. Each Method 6B sample obtained over 24 hours represents 24 1-hour averages. If Method 6A or 6B is used under paragraph (i) of this section, the conditions under §60.46(d)(1) apply; these conditions do not apply under paragraph (h) of this section.
- (2) For Method 7, Method 7A, 7C, 7D, or 7E may be used. If Method 7C, 7D, or 7E is used, the sampling time for each run shall be 1 hour.
- (3) For Method 3, Method 3A or 3B may be used if the sampling time is 1 hour.
- (4) For Method 3B, Method 3A may be used.

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§ 60.48a Compliance determination procedures and methods.

- (a) In conducting the performance tests required in $\S60.8$, the owner or operator shall use as reference methods and procedures the methods in appendix A of this part or the methods and procedures as specified in this section, except as provided in $\S60.8$ (b). Section 60.8(f) does not apply to this section for SO_2 and NO_x . Acceptable alternative methods are given in paragraph (e) of this section.
- (b) The owner or operator shall determine compliance with the particulate matter standards in §60.42a as follows:
- (1) The dry basis F factor (O_2) procedures in Method 19 shall be used to compute the emission rate of particulate matter.
- (2) For the particular matter concentration, Method 5 shall be used at affected facilities without wet FGD systems and Method 5B shall be used after wet FGD systems.
- (i) The sampling time and sample volume for each run shall be at least 120 minutes and 1.70 dscm (60 dscf). The probe and filter holder heating system in the sampling train may be set to provide an average gas temperature of no greater than $160\pm14~^{\circ}\text{C}$ ($320\pm25~^{\circ}\text{F}$).

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- (ii) For each particulate run, the emission rate correction factor, integrated or grab sampling and analysis procedures of Method 3B shall be used to determine the O2 concentration. The O2 sample shall be obtained simultaneously with, and at the same traverse points as, the particulate run. If the particulate run has more than 12 traverse points, the O_2 traverse points may be reduced to 12 provided that Method 1 is used to locate the 12 O2 traverse points. If the grab sampling procedure is used, the O₂ concentration for the run shall be the arithmetic mean of all the individual O2 concentrations at each traverse point.
- (3) Method 9 and the procedures in §60.11 shall be used to determine opacity.
- (c) The owner or operator shall determine compliance with the SO_2 standards in $\S 60.43a$ as follows:
- (1) The percent of potential SO_2 emissions (%P_s) to the atmosphere shall be computed using the following equation:

 $P_s = [(100 - R_f) (100 - R_g)]/100$

where:

 P_s =percent of potential SO_2 emissions, percent.

 R_f =percent reduction from fuel pretreatment, percent.

 R_g =percent reduction by SO_2 control system, percent.

- (2) The procedures in Method 19 may be used to determine percent reduction ((R_f)) of sulfur by such processes as fuel pretreatment (physical coal cleaning, hydrodesulfurization of fuel oil, etc.), coal pulverizers, and bottom and flyash interactions. This determination is optional.
- (3) The procedures in Method 19 shall be used to determine the percent SO_2 reduction (% R_g of any SO_2 control system. Alternatively, a combination of an "as fired" fuel monitor and emission rates measured after the control system, following the procedures in Method 19, may be used if the percent reduction is calculated using the average emission rate from the SO_2 control device and the average SO_2 input rate from the "as fired" fuel analysis for 30 successive boiler operating days.
- (4) The appropriate procedures in Method 19 shall be used to determine the emission rate.

- (5) The continuous monitoring system in $\S 60.47a$ (b) and (d) shall be used to determine the concentrations of SO_2 and CO_2 or O_2 .
- (d) The owner or operator shall determine compliance with the NO_x standard in $\S 60.44a$ as follows:
- (1) The appropriate procedures in Method 19 shall be used to determine the emission rate of NO_x .
- (2) The continous monitoring system in $\S 60.47a$ (c) and (d) shall be used to determine the concentrations of NO_x and CO₂ or O₂.
- (e) The owner or operator may use the following as alternatives to the reference methods and procedures specified in this section:
- (1) For Method 5 or 5B, Method 17 may be used at facilities with or without wet FGD systems if the stack temperature at the sampling location does not exceed an average temperature of $160~^{\circ}\text{C}$ ($320~^{\circ}\text{F}$). The procedures of §§2.1 and 2.3 of Method 5B may be used in Method 17 only if it is used after wet FGD systems. Method 17 shall not be used after wet FGD systems if the effluent is saturated or laden with water droplets.
- (2) The F_c factor (CO₂) procedures in Method 19 may be used to compute the emission rate of particulate matter under the stipulations of \$60.46(d)(1). The CO₂ shall be determined in the same manner as the O₂ concentration.
- (f) Electric utility combined cycle gas turbines are performance tested for particulate matter, sulfur dioxide, and nitrogen oxides using the procedures of Method 19 (appendix A). The sulfur dioxide and nitrogen oxides emission rates from the gas turbine used in Method 19 (appendix A) calculations are determined when the gas turbine is performance tested under subpart GG. The potential uncontrolled particulate matter emission rate from a gas turbine is defined as 17 ng/J (0.04 lb/million Btu) heat input.

[44 FR 33613, June 11, 1979, as amended at 54 FR 6664, Feb. 14, 1989; 55 FR 5212, Feb. 14, 1990]

§60.49a Reporting requirements.

(a) For sulfur dioxide, nitrogen oxides, and particulate matter emissions,